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Biotechnology can be used to convert waste into valuable products. In this context, there is bacterial cellulose (BC), a natural biopolymer that can be transformed into several useful materials, but its production is limited due to the high cost of the culture media used for its industrialization. In this work, BC was produced from the bacteria *Komagataeibacter rhaeticus*, using coffee grounds, sugarcane molasses and ethanol. The experiments were carried out under static conditions. The products were collected every 48 h, with a total period of 240 h. The maximum BC production (11.08 g.L⁻¹) was obtained in a culture medium supplemented with coffee powder, hydrolyzed cane molasses and the addition of 1% (v/v) ethanol. The results show that the use of different carbon sources of the evaluated by-products are viable alternatives in reducing costs in BC production.

Keywords: Bacterial cellulose, Biopolymer, Coffee grounds, Komagataeibacter rhaeticus, Sugarcane molasses.

1. Introduction

Represented by the formula $(C_6H_{10}O_5)_n$, cellulose is a polysaccharide formed by β -D-glucopyranose units linked by β -(1 \rightarrow 4) glycosidic bonds and can be found in different types of living organisms. When bacteria of the genus *Komagataeibacter* are grown under static conditions, they can excrete cellulose on the surface of the medium as a layer of jelly¹⁻³. This non-toxic biopolymer has a high potential for liquid retention, an important property for medical and tissue engineering applications. Bacterial cellulose (BC) has characteristics similar to vegetable cellulose (VC). However, BC has different degrees of polymerization and means of production. BC fibers are more stable and more resistant due to their ultra-fine reticular structure, high crystallinity, high tensile strength, high elasticity and durability⁴⁻⁶.

Due to the excellent physical and chemical properties, the use of BC arouses great interest in various applications. Food packaging⁷, scaffolding engineering⁸, electronic devices⁹, textile industries¹⁰, and even artificial blood vessels¹¹, as well as application in pharmaceuticals as a drug delivery system¹²

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and cosmetics industry¹³, are some of the many examples of possible BC applications on an industrial scale¹⁴. BC production can be carried out by several gram-negative bacteria, among which those belonging to the genus *Gluconacetobacter xylinus* stand out as the main producers in many studies for commercial purposes¹⁵. To make BC production more economically efficient, it is important to use other bacteria that appear as alternatives to optimize production time, reduce costs and generate products with similar physicochemical properties. In this context, the bacterium *Komagataeibacter rhaeticus* appears as a viable alternative¹⁶.

Another aspect related to the high cost of production refers to the culture medium used in the process. Different sources of carbon, such as mannitol, sorbitol, fructose, glycerol, among others, can be used by the bacterium *Komagataeibacteria rhaeticus*. However, glucose is the most common, as it is the main source used in the standard production medium Hestrin & Schramm¹⁷. In literature, studies have found alternative carbon sources, such as sugarcane molasses¹⁶, by-products from the biodiesel industry and residues from the confectionery industries¹⁸ and tropical fruit residues¹⁹. Among these alternatives, there is the combination of sugarcane molasses and coffee grounds as alternative carbon sources. Cane molasses is a by-product of sugar production and has large amounts of fermentable sugars such as fructose, sucrose and glucose²⁰. In addition, Brazil is the largest producer of sugarcane and sugar in the world, and is among the largest exporters of this product²¹. In relation to coffee, due to its huge production and consumption on a global scale, a considerable amount of coffee grounds powder residues is generated, which are harmful to the environment²². The use of this residue in the production of a biopolymer would help to reduce environmental pollution, in addition to promoting new alternatives to take advantage of its high organic content.

In this context, the present study aimed to produce bacterial cellulose films using a medium composed of nutritious and low-cost sources, such as sugarcane molasses (SCM) and coffee grounds (CG), and determine the kinetic parameters met in the process.

2. Materials and Methods

2.1. Preparation of lineage keeping and inoculum medium

The microorganism used was *Komagataeibacter rhaeticus*, isolated in the Microbiology Laboratory of the Department of Chemical Engineering at UFPE, and identified in the Microorganism Collection sector - UFPEDA (UFPE). The medium used to maintain the inoculum was a modified Hestrin and Schramm¹⁷: Yeast Extract (5.0 g.L⁻¹), Peptone (5.0 g.L⁻¹), Na₂HPO₄ (2.7 g.L⁻¹), Citric Acid Monohydrate (1.15 g.L⁻¹), Agar-Agar (20.05 g.L⁻¹) and SCM as the main carbon source (40 g.L⁻¹). The pH of the medium was adjusted to 6.0.

2.2. Inoculum preparation

The medium prepared for the inoculum growth was 250 mL according to Hestrin & Schramm¹⁷, where the carbon source was modified: Yeast Extract (5.0 g.L⁻¹), Peptone (5.0 g.L⁻¹), Na₂HPO₄ (2.7 g.L⁻¹), Citric Acid Monohydrate (1.15 g.L⁻¹) and SCM was used as the main carbon source (40 g.L⁻¹). After adjusting the pH (6.0) using sodium hydroxide/hydrochloric acid, the medium was transferred to a 500 mL Erlenmeyer to be sterilized in an autoclave at 121 °C for 15 min. After the cooling process, 0.6 g.L⁻¹ of *Komagataeibacter Rhaeticus* cells were aseptically transferred to the inoculum in a shaker at 30 ° C for 2 days with a rotation speed of 120 rpm.

2.3. Bacterial cellulose production

Three culture media called (A), (A1), (B), (B1), (C) and (C1) were prepared. They consist of the following components: CG (8 g.L⁻¹) and crude SCM (150 g.L⁻¹); crude SCM (150 g.L⁻¹); CG (8 g.L⁻¹) and hydrolyzed SCM (150 g.L⁻¹); hydrolyzed SCM (150 g.L⁻¹); CG (8 g.L⁻¹), hydrolyzed SCM (150 g.L⁻¹) and 1% v/v ethanol; and hydrolyzed SCM (150 g.L⁻¹) and 1% v/v ethanol, respectively.

In culture medium (A) preparation, 4 g of SCM dissolved in 500 ml of distilled water and 75 g of CG dispersed in 500 ml of distilled water were mixed. The total volume of the culture medium was 1 liter. The pH of this medium was adjusted to 4.0 using a 1M HCl solution. This culture medium was distributed to 5 Roux flasks. 90 ml of the culture medium was transferred to each flask. These flasks were closed and sterilized in an autoclave at 121 °C for 15 min. After cooling the culture media, 10 mL of inoculum was transferred to each Roux flask. Culture medium (A) final volume, in each Roux flask, was 100 ml. The flasks were incubated in a static system for 240 hours. The bacterial cellulose films produced were collected every 48 h, purified and weighed.

Culture media (B) and (C), have a similar procedure to the preparation of culture medium A, except with the prehydrolysis stage of sucrose present in sugarcane molasses. For culture media B and C preparation, the hydrolysis of sucrose present in cane molasses was carried out. For this, 4 g of cane molasses was dissolved in 500 mL of distilled water. The pH of this mixture was adjusted to 2.0 using a 1M HCl solution. This mixture was placed in a water bath at 67 °C for 15 min. Upon completion of hydrolysis, the CG dispersed in 500 mL of distilled water was added. Culture medium total volume was 1 liter. The pH of this medium was adjusted to 4.0 using a 1M HCl solution. This culture medium was distributed to 5 Roux flasks and 90 ml was transferred to each flask. They were closed and sterilized in an autoclave at 121 °C for 15 min. After cooling the culture media, 10 mL of inoculum was transferred to each Roux flask. Culture medium (B) final volume in each Roux flask was 100 ml. For culture medium (C), 10 ml of inoculum and then 1% ethanol in relation to the total volume (100 ml) were added, which corresponds to 1 ml of ethanol. Culture medium (C) final volume, in each Roux flask, was 101 mL. The flasks were incubated in a static system for 240 hours. The bacterial cellulose films produced were collected every 48 h, purified and weighed.

Culture media (A1), (B1) and (C1) were produced following the same methodology as culture media (A), (B) and (C), with the difference that coffee grounds were not used in these media. The bacterial cellulose films produced in these systems were collected at the end of the 240 h period for weighing the biopolymer.

2.4. Kinetics parameters

The biopolymers produced were washed with distilled water and subjected to treatment with 0.1 M sodium hydroxide (NaOH) for 24 h at 80 °C in a water bath, under static conditions, and then dried at 50 °C for 48 hours. To determine the substrate conversion factor in the product and the productivity, Equations 1 and 2²³ were used, respectively.

$$Y_{P/S} = \frac{P_f - P_i}{S_i - S_f} \tag{1}$$

$$PR = \frac{P_f}{t} \tag{2}$$

Where: P_f is the final concentration of the product (g.L⁻¹); P_i is the initial concentration of the product; S_f is the final concentration of the substrate; S_i is the initial substrate concentration; t is the total process time (h); $Y_{P/S}$ is a conversion factor of the substrate in the product; and PR is productivity. The substrates (S) are the free monosaccharides (glucose and/ or fructose) in the culture medium. The product (P) is bacterial cellulose. Time (t) is the total production period (240 h).

The determination of total sugar reduction was performed using the DNS method (3,5-Dinitrosalicylic acid)²⁴. This method consists of reducing, in an alkaline medium, 3-amino-5-nitrosalicylic acid (DNS) by the action of reducing sugars. To perform the quantification of hydrolysable sugars by the DNS method, the following steps were performed: 1 mL of molasses was hydrolyzed with HCl at 68 °C for 15 min; the solution was cooled and neutralized with NaOH and then diluted; of this solution, 0.5 mL was transferred to the Folin Wu tube and 1 ml of DNS was added; this system was heated to 100°C for 5 min; this solution was measured with distilled water to the total volume of 12.5 mL and the transmittance reading was performed on the Edutec model Q798DP UV-VIS spectrophotometer at a wavelength of 540 nm.

3. Results and Discussion

3.1. Kinetic study of the medium

Table 1 shows the results of bacterial cellulose production with the following culture media evaluated: medium (A) (CG and crude SCM), medium (A1) (crude SCM), medium (B) (CG and hydrolyzed SCM), medium (B1) (hydrolyzed SCM), medium (C) (CG, hydrolyzed SCM and ethanol) and medium (C1) (hydrolyzed SCM and ethanol) at various times.

Culture media (A) and (A1) showed the lowest bacterial cellulose production with or without the addition of SG. When compared with the other culture media evaluated, it appears that the hydrolyzed SCM, present in culture media (B), (B1), (C) and (C1), contributed to higher yields in the biopolymer production. This is justified by the fact that fermentable sugars contribute to increase cellulose production, which makes it important to carry out a process of hydrolysis in the disaccharide residues or other carbohydrates so that better cellulose yields are achieved²⁵⁻²⁷.

Culture medium (C) showed the highest bacterial cellulose production during the entire process (240 h). This is justified by the combination of hydrolyzed sucrose, coffee grounds and the addition of ethanol to the culture medium. CG is rich in polysaccharides, oils, proteins and substances that can also influence the production of bacterial cellulose^{28,29}. Ethanol, on the other hand, acts as an energy source for the generation of adenosine triphosphate (ATP) and increases the flow of glucose 6-phosphate (G6P) (precursor to BC) in the bacterial cellulose biosynthetic route. This solvent acts as an activator in cell growth and depending on the concentration may favor the production of bacterial cellulose28,30. This results in the effective use of glucose for the cellulose synthesis and not in its use for the acquisition of energy³¹. The great contribution of ethanol in the bacterial cellulose production can be seen in Figure 1, when graphically comparing the productions of biopolymer during the period from 0 to 240 h for culture media (A), (B) and (C). In the period of 240 h, it appears that culture medium (C) had a biopolymer production 6 times greater than medium (A) and 4 times greater than culture medium (B).

 Table 1. Monitoring the production of biopolymer in the culture media evaluated at various times.

Produced	Time (h)					
biopolymer (g.L-1)	0	48	96	144	192	240
Culture medium (A)	0	0.61	1.13	1.30	1.76	1.79
Culture medium (A1)	0	-	-	-	-	1.05
Culture medium (B)	0	1.60	1.64	1.66	2.15	2.63
Culture medium (B1)	0	-	-	-	-	1.70
Culture medium (C)	0	4.33	7.20	8.08	8.89	11.08
Culture medium (C1)	0	-	-	-	-	6.50

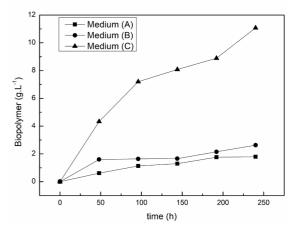


Figure 1. Production of bacterial cellulose as a function of the time for the culture media (A), (B) and (C).

Analyzing the contribution of coffee grounds in cellulose production, it appears that the nutrients present favored the production of bacterial cellulose. This can be verified by the yields in Table 1. Comparing the yields of culture medium (A) and (A1) in the total production period (240 h), it can be seen that there was a 59% increase in bacterial cellulose yield. In relation to culture media (B) and (B1), there was a 65% increase in the bacterial cellulose production. Comparing the culture media (C) and (C1) that had the addition of ethanol, there was also a 59% increase in bacterial cellulose production.

The amount of CG that is generated worldwide is very high³², which reinforces the importance of valuing this lowcost nutritional source in this polysaccharide production. In addition, CG can also be evaluated in other industrial bioprocesses. In literature, there are studies that used sugarcane molasses as a carbon source in bacterial cellulose production. No studies were found that used coffee grounds as a carbon source to produce bacterial cellulose.

Rodrigues et al.³³ studied the production of bacterial nanocellulose using the bacteria *Komagataeibacter xylinus* BPR 2001 and low-cost substrates such as molasses, ethanol, corn steep liquor (CSL) and ammonium sulfate. The results showed that the composition of molasses 5.38, CSL 1.91, ammonium sulfate 0.63, disodium phosphate 0.270, citric acid 0.115 and ethanol 1.38% (v/v) result in a high yield of bacterial cellulose. Machado et al.²⁰ studied the production of bacterial cellulose using the bacteria *Komagataeibacter rhaeticus* using sugarcane molasses (SCM) (totally or partially) without previous treatment, as an alternative carbon source. The membranes obtained showed characteristics similar to

those obtained from conventional medium of Hestrin and Schramm and the partial substitution of glucose by the sources of nutrients present in the molasses (sucrose, fructose and glucose) do not affect the BC production capacity. Tyagi and Suresh³⁴ studied the production of bacterial cellulose using *Gluconacetobacter intermedius* SNT-1 using acid-treated molasses. The results showed that the yields were relatively lower compared to the HS medium containing glucose as a carbon source. Bae and Shoda³⁵ studied the production of bacterial cellulose by *Acetobacter xylinum* BPR2001 using SCM as a low-cost carbon source. The cane molasses was subjected to heat treatment with H_2SO_4 . The results showed that the maximum BC concentration for this treated molasses increased 76% and the specific growth rate increased 2 times in comparison with that of non-hydrolyzed molasses.

Figures 2, 3 and 4 illustrate the kinetic profiles of the total reduction sugars (TRS) consumption versus the production of biopolymer during the period from 0 to 240 h for culture media (A), (B) and (C).

In Figures 2 and 3, it can be seen, from the curves, that the low production of bacterial cellulose is possibly due to the use of this carbon source for the formation of other noncellulosic metabolites. Without the presence of ethanol, glucose competes in cellulose synthesis and glucose oxidation³⁶. In Figure 2, it is also observed that there is a stabilization of the polymer production curve after 192 h. This may have been caused by the low amount of glucose and nutrients needed to produce BC after that time. In Figure 3, there is also a tendency towards this same behavior. However, it appears that in the interval of 192 to 240 hs, there is a stabilization of the amount of glucose, but the biopolymer production increases, showing that nutrients are still available in the culture medium. In the kinetic curve of Figure 4, it turns out that there was a shift in glucose consumption to BC biosynthesis. This can be verified by the production throughout the biosynthesis process. This was caused by ethanol that increases the flow of glucose-6-phosphate (G6P) in the metabolic pathway for BC synthesis and causes a reduction in glucose-6-phosphate dehydrogenase (G6PDH) activity, which causes inhibition of the pathway of phosphate pentoses³⁷.

From Figures 2, 3 and 4 it was possible to determine the kinetic parameters, which are presented in Table 2.

The best result for the productivity parameter in this work was 0.046 g.L⁻¹.h⁻¹ for culture medium (C). However, when compared to the literature, other authors such as Bae and Shoda³⁵, used SCM (40 g.L⁻¹) treated with H₂SO₄ and reached a BC production of 0.074 g.L⁻¹.h⁻¹. Jaramillo et al.³⁸, studied the effect of sucrose during the production of BC on static cultivation and obtained productivity of 0.0480 g.L⁻¹.h⁻¹ with a sucrose concentration of 1.7% (w/v). In addition, Çakar et al.³⁹, reported the improvement of BC production in a semi-continuous process in a medium containing SCMs and obtained a maximum production of 0.0024 g.L⁻¹.h⁻¹ BC.

Therefore, it can be said that SCM enriched with CG in the presence of ethanol, contains many nutrients that are favorable to microbial growth, in addition to ethanol that acts as an enhancer for bacterial cellulose production. This shows that CG can be a promising and low-cost alternative for the biopolymer production.

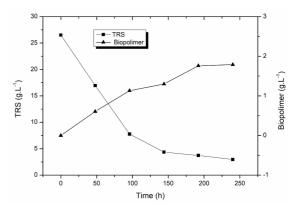


Figure 2. Kinetic curves based at the concentration of total reducing sugars for the culture medium (A).

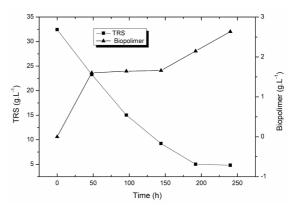


Figure 3. Kinetic curves based at the concentration of total reducing sugars for the medium (B).

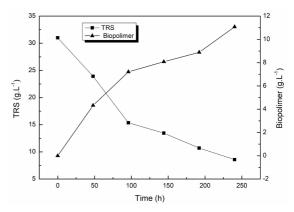


Figure 4. Kinetic curves based at the concentration of total reducing sugars for the culture medium (C).

 Table 2. Results of the kinetic parameters of the culture media evaluated.

Parameter -	Results					
	Medium (A)	Medium (B)	Medium (C)			
$Y_{P/S}$	0.076	0.095	0.494			
PR (g.L ⁻¹ .h ⁻¹)	0.007	0.011	0.046			

4. Conclusions

The kinetic study of bacterial cellulose production using sugarcane molasses and coffee grounds was satisfactory. From the results, it was verified that sugarcane molasses hydrolysis increases in the biopolymer production. However, the combination of sugarcane molasses and coffee grounds provided extra nutrients to the medium, in addition to ethanol supplementation, showing that the synergistic action of these three components increases the production of bacterial cellulose. From this study, it was found that the addition of coffee grounds proved to be a valuable nutrient for the metabolism of BC production. It is believed that new studies on the topic are very promising since the production of BC in the presence of CG and SCM can still be optimized. Other factors of production can still be investigated, such as the maximum production time for the total conversion of the substrate into product and the use of batch fermentations.

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